

# Viscosity

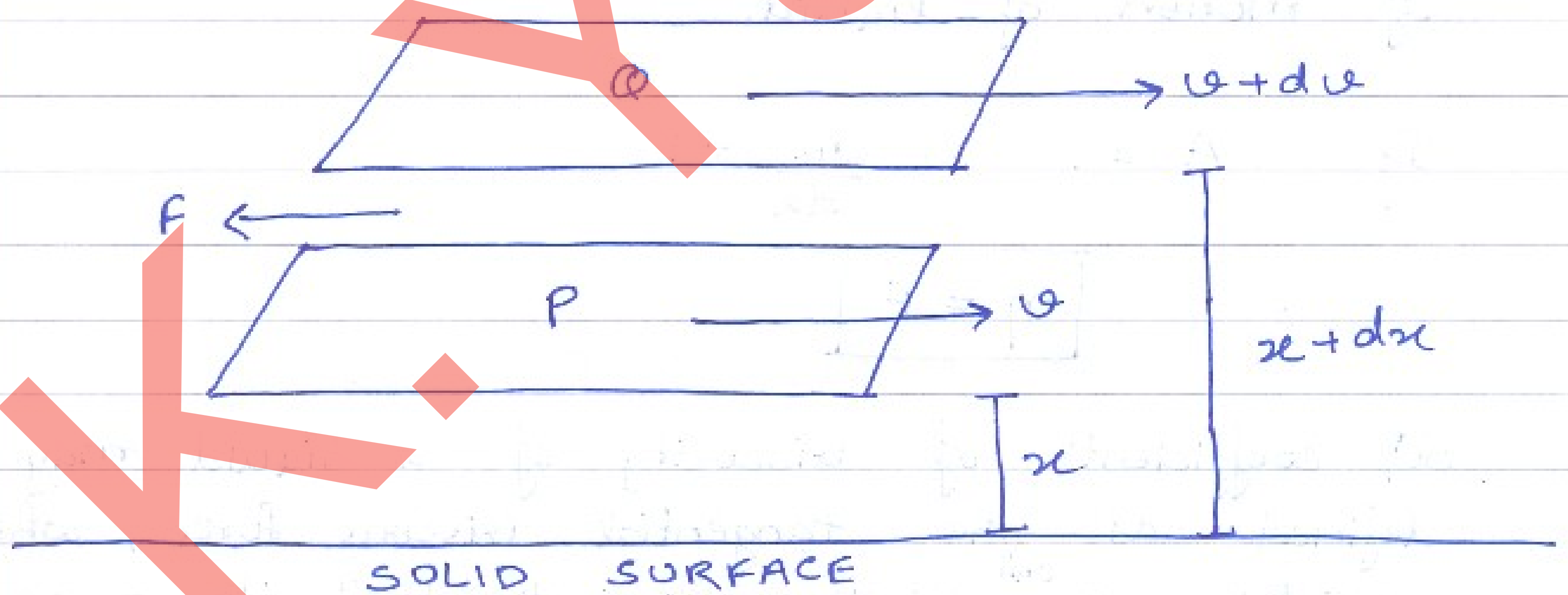
## Viscosity

The property of fluids by virtue of which an internal resistance or friction comes into play, when a fluid is in motion is called viscosity.

OR

The property of fluids by virtue of which a backward dragging force acts tangentially on the layers of the fluid in motion & it tries to stop the motion is called viscosity.

## Coefficient of Viscosity ( $\eta$ )



Consider 2 parallel layers P & Q at distances  $x, x + dx$  from the solid surface moving with velocities  $v$  &  $v + dv$  resp.

The relative motion bet<sup>n</sup> the 2 layers can take place only if some external force acts bet<sup>n</sup> them.

Due to viscosity, a force  $F$  acts in opposite direction to the relative motion.

Acc. to Newton, the viscous force  $F$  depends on

(a) area of layers in contact

$$F \propto A$$

(b) velocity gradient bet<sup>n</sup> layers

$$F \propto \frac{dv}{dx}$$

$$\therefore F \propto A \frac{dv}{dx}$$

$$F = -\eta A \frac{dv}{dx}$$

-ve sign shows that the viscous force is directed in a direction opp. to the direction of motion of liquid.

If  $A = 1$  &  $\frac{dv}{dx} = 1$

$$\eta = F$$

So, coefficient of viscosity of a liquid may be defined as the tangential viscous force, which maintains a <sup>unit</sup> velocity gradient bet<sup>n</sup> its 2 parallel layers, each of unit area.

Unit of  $\eta$

S.I. unit - poiseuille (Pl)

$$1 \text{ Pl} = 1 \text{ Nm}^{-2} \text{ s}$$

c.g.s unit - poise

$$1 \text{ poise} = 1 \text{ dyne cm}^{-2} \text{ s}$$

$$1 \text{ Pl} = 1 \text{ Nm}^{-2} \text{ s} = 10^5 \text{ dyne} \times (100 \text{ cm})^{-2} \text{ s}$$

$$= 10 \text{ dyne cm}^{-2} \text{ s}$$

$$1 \text{ Pl} = 10 \text{ poise}$$

## Similarity bet<sup>n</sup> solid friction & viscosity

- ① Both opposes motion
- ② comes into play whenever there is relative motion
- ③ Both are due to molecular attractions.

## Differences

- ① Solid friction - independent of area in contact  
viscosity - proportional to surface area
- ② Solid friction - independent of tem.  
viscosity - decreases with tem.

Q. How is the knowledge of  $\eta$  helps in selecting a suitable lubricant for a machine?

Ans The knowledge of  $\eta$  of different liquids & its variation with tem. helps in selecting a suitable lubricant for a machine.

## Poiseuille's formula for flow of liquid through a capillary tube

Poiseuille found that volume of liquid flowing per sec. ( $V$ ) is

$$V \propto p \quad \text{[pressure diff. at 2 ends]}$$

$$V \propto r^4 \quad \text{[radius of tube]}$$

$$V \propto \frac{1}{l} \quad \text{[length of tube]}$$

$$V \propto \frac{1}{\eta}$$

So,  $V \propto \frac{p r^4}{\eta l} \Rightarrow \boxed{V = \frac{\pi}{8} \frac{p r^4}{\eta l}}$

## Stoke's law

- When a spherical body falls through the fluid, layer in immediate contact with it, sticks to it, & moves along the body with same velocity
- The layer next to it has lesser velocity, the next still lesser & so on.
- As a result of this, a backward dragging force called viscous force ( $F$ ) is set up, which opposes the motion of the body.
- As the velocity goes on increase,  $F$  also increases & becomes equal to weight of the body.
- Then the body moves with a constant velocity called terminal velocity ( $v$ )
- Acc. to Stoke  
 "When a body attains terminal velocity, then the viscous force on the body is  

$$F = 6\pi\eta r v$$

Proof:

Let  $F \propto \eta^a r^b v^c$

$$F = k \eta^a r^b v^c$$

$$[MLT^{-2}] = k [ML^{-1}T^{-1}]^a [L]^b [LT^{-1}]^c$$

$$= [M]^a [L]^{-a+b+c} [T]^{-a-c}$$

$$a = 1$$

$$-a+b+c = 1$$

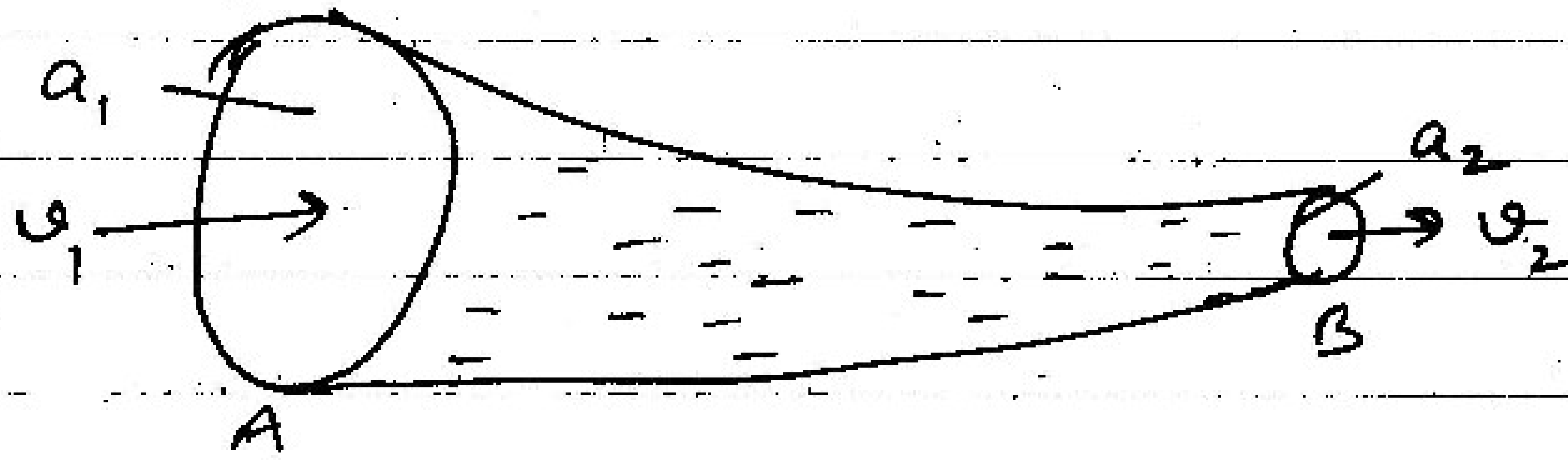
$$-a-c = -2 \Rightarrow c = 1$$

$$b = 1$$

$$F = k \eta r v \Rightarrow \boxed{F = 6\pi\eta r v}$$

# Fluid Flow

## Eq<sup>n</sup> of continuity



Consider a liquid moving through a pipe AB of varying cross-section.

Let  $a_1$  - cross-sectional area of pipe at A  
 $a_2$  - " " " " " B  
 $v_1$  - ~~enter~~ entering velocity of liquid at A  
 $v_2$  - exist " " " " B.  
 $\rho_1$  - density of liquid at A  
 $\rho_2$  - " " " " B

Volume of liquid entering per sec. at A =  $a_1 v_1$   
 $\therefore$  Mass of liquid entering per sec. at A =  $a_1 v_1 \rho_1$   
 " " " " " B =  $a_2 v_2 \rho_2$

As there is no source or sink of liquid along the length of pipe, the mass of liquid crossing any section of pipe is same  
 i.e.  $a_1 v_1 \rho_1 = a_2 v_2 \rho_2$

Now,  $\rho_1 = \rho_2$  (as the liquid is incompressible)

$$a_1 v_1 = a_2 v_2$$

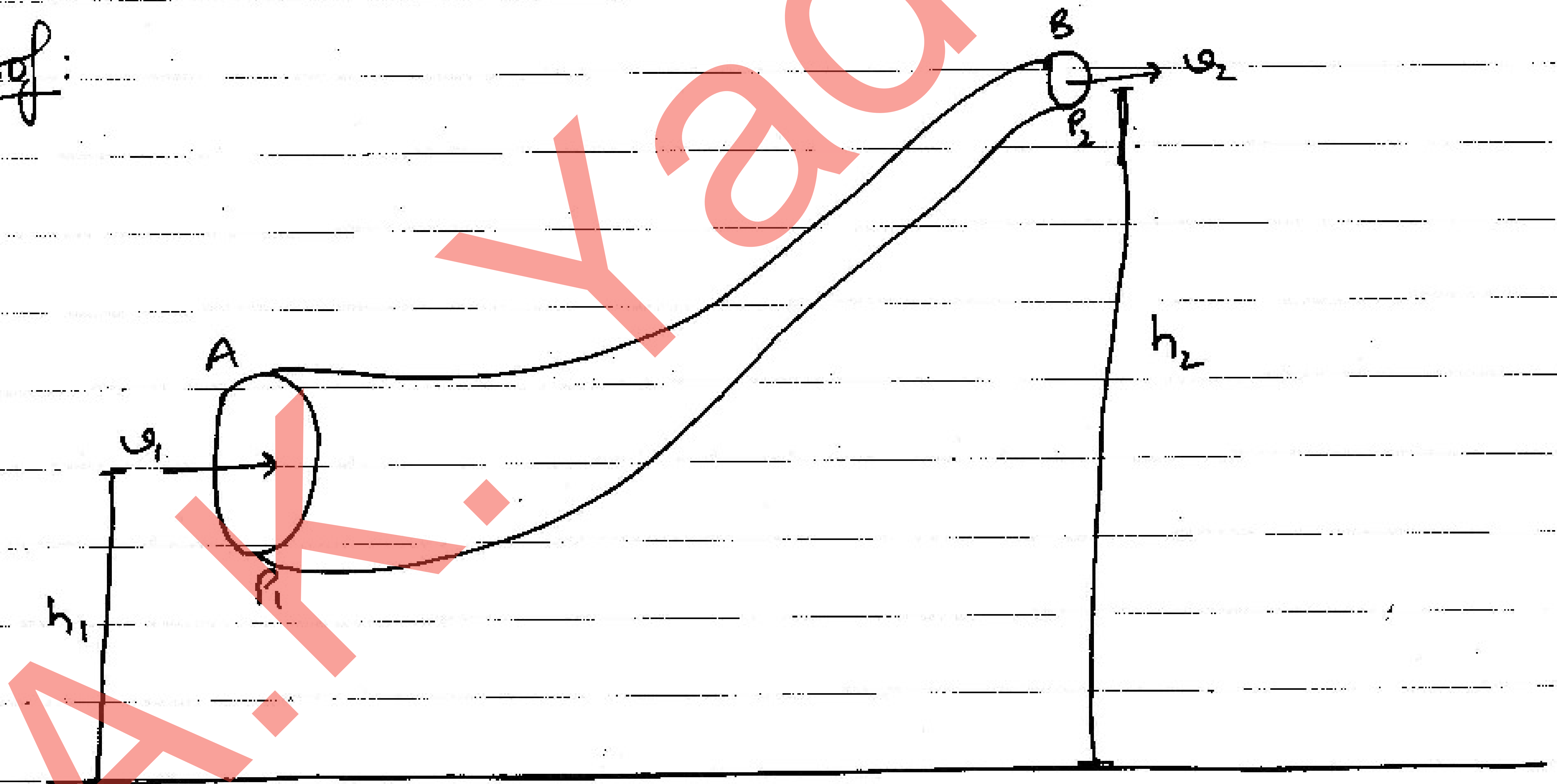
## Bernoulli's theorem

The total energy (pressure energy, potential energy & kinetic energy) of an incompressible and non-viscous fluid in steady flow through a pipe remains constant throughout the flow, provided there is no source or sink of fluid along the length of the pipe.

Mathematically, for a unit mass of fluid

$$\frac{P}{\rho} + gh + \frac{1}{2}v^2 = \text{const.}$$

Proof:



Consider a tube AB of varying cross-section through which an ideal liquid is in streamline flow.

Let  $P_1, P_2$  - pressure at A & B

$a_1, a_2$  - area of cross-section of tube at A & B

$h_1, h_2$  - mean height of A & B from ground

$v_1, v_2$  - velocity of liquid at A & B

$\rho$  - density of ideal liquid flowing through the tube.

Also,  $P_1 > P_2$

Acc. to eq<sup>n</sup> of continuity, the mass  $m$  of the liquid crossing per sec. through any section of the tube is

$$a_1 v_1 \rho = a_2 v_2 \rho = m$$

$$a_1 v_1 = a_2 v_2 = \frac{m}{\rho} = V$$

As  $a_1 > a_2$  so  $v_2 > v_1$

Work done per sec. on the liquid by the pressure energy at A =  $P_1 a_1 \times v_1 = P_1 V$

Work done per sec. by the liquid against the pressure energy at B =  $P_2 a_2 \times v_2 = P_2 V$

Net work done per sec. on the liquid by the pressure energy in moving the liquid from A to B =  $P_1 V - P_2 V$

Increase in P.E./sec. of liquid from A to B =  $mgh_2 - mgh_1$

" " " " " " " " " " " " =  $\frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2$

Acc. to work energy theorem

Work done/sec. on the liquid by pressure energy = increase in P.E./sec. + increase in K.E./sec.

$$P_1 V - P_2 V = (mgh_2 - mgh_1) + \left( \frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2 \right)$$

$$P_1 V + mgh_1 + \frac{1}{2} m v_1^2 = P_2 V + mgh_2 + \frac{1}{2} m v_2^2$$

$$\frac{P_1 V}{m} + gh_1 + \frac{1}{2} v_1^2 = \frac{P_2 V}{m} + gh_2 + \frac{1}{2} v_2^2$$

$$\frac{P_1}{\rho} + gh_1 + \frac{1}{2} v_1^2 = \frac{P_2}{\rho} + gh_2 + \frac{1}{2} v_2^2$$

$$\boxed{\frac{P_0}{\rho} + gh + \frac{1}{2} v^2 = \text{const.}}$$

### Limitations of Bernoulli's theorem

1. It was incorrectly assumed that velocity of liquid across any cross-section of tube is uniform.
2. The viscous drag force comes into play when the liquid is in motion, has not been taken into account.
3. While deriving the eq<sup>n</sup>, it is <sup>wrongly</sup> assumed that there is no loss of energy when the liquid is in motion.
4. If the liquid is flowing along a curved path, the energy due to centrifugal force should also be considered.



## Applications of Bernoulli's theorem

### ① Atomiser

Air blowing out of the bulb creates low pressure so liquid rises up from high pressure region to low pressure acc. to Bernoulli's theorem.

### ② Lift on aeroplane wing (aerofoil)

- The upper surface is more curved than the lower surface & head is more thicker than tail.
- As upper surface is more curved than lower surface so speed of air above the wings is more.
- According to Bernoulli's theorem pressure above the wings will be less.
- Due to this pressure difference on the two sides of the wings, a vertical lift acts on the aeroplane.

### ③ Magnus effect

- When a ball is spinning as well as moving linearly, the streamlines at the top of the ball are opposite to each other and those below are in same direction.
- As a result, the velocity of air flow is greater below than above the ball.
- Acc. to Bernoulli's theorem, the pressure on upper side of ball becomes more than the pressure on the lower side of the ball.
- Due to it, a resultant force acts on

the ball at right angles to the linear motion in the downward direction, resulting the ball to move along a curved path.

- This dynamic force due to spinning of ball is called Magnus effect.

④ Blowing off the roofs during storm.

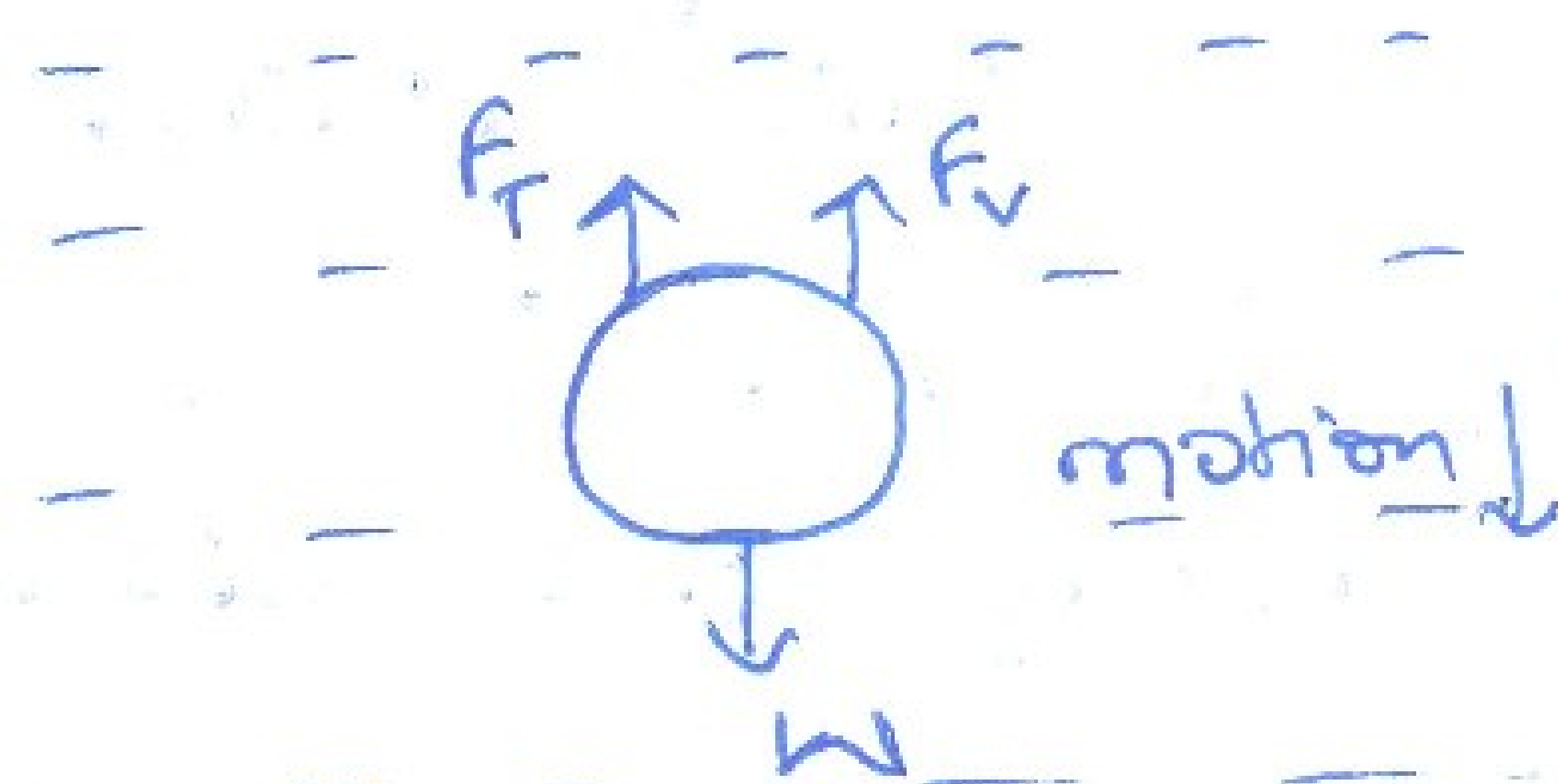
⑤ Motion of two parallel boats.

AKY paper

## Terminal velocity

It is the max. constant velocity acquired by the body while falling freely in a viscous medium.

Consider a small spherical body falling freely in a viscous medium.



The forces acting on the body are

- (i) Weight ( $W$ ) of the body acting downwards
- (ii) Upthrust ( $F_T$ ) equal to weight of liquid displaced.
- (iii) Viscous drag force ( $F_v$ ) acting upwards

Let  $\rho$  - density of material of the spherical body  
 $r$  - radius of spherical body  
 $\sigma$  - density of medium

Weight of the body,  $W = V \times \rho \times g$   
 $= \frac{4}{3} \pi r^3 \rho g$

Upthrust due to buoyancy,  $F_T = V \times \sigma \times g$   
 $= \frac{4}{3} \pi r^3 \sigma g$

Upward viscous drag force,  $F_v = 6\pi\eta r v$

When body attains terminal velocity

$$F_T + F_v = W$$

$$\frac{4}{3} \pi r^3 \sigma g + 6\pi\eta r v = \frac{4}{3} \pi r^3 \rho g$$

$$6\pi\eta r v = \frac{4}{3} \pi r^3 (\rho - \sigma) g$$

$$v = \frac{2}{9} \frac{r^2 (\rho - \sigma) g}{\eta}$$

## Conclusion

- (i) If  $\rho < \sigma$ ,  $v = \text{negative}$
- Body will move up with a constant velocity.
  - Example - gas bubbles rise up through soda water bottle.
- (ii) If  $\rho > \sigma$ ,  $v = \text{positive}$
- Body will attain terminal velocity in downward direction
- (iii) If  $\rho = \sigma$ ,  $v = 0$
- Body remains suspended in the medium.

## Variation of Viscosity

### ① Increase in tem.

viscosity of liquids - decreases  
" " gases - increases

### ② Increase in pressure

viscosity of liquids - increases  
" " water - decreases  
" " gases - unchanged

## Streamline, Laminar & Turbulent Flow

Streamline flow - The flow in which every particle of the liquid follows exactly the path of its preceding particle & has the same velocity in magnitude & direction as that of its preceding particle while crossing through that point.

Laminar flow - Flow in which the liquid moves in layers.

Turbulent flow - When a liquid moves with a velocity greater than its critical velocity, the motion of the particles of liquid becomes disorderly. Such a flow is called turbulent flow.

## Reynold's number ( $N_R$ )

It is a pure number which determines the nature of flow of liquid through a pipe.

$$N_R = \frac{\rho D v_c}{\eta}$$

where  $\rho$  - density of liquid  
 $D$  - diameter of tube  
 $v_c$  - critical velocity  
 $\eta$  - coefficient of viscosity of liquid

- $N_R = 0$  to  $2000$  - stream line or laminar
- $N_R = 2000$  -  $3000$  - unstable
- $N_R > 3000$  - turbulent.

•  $N_R$  is independent of the system of units used for the measurement of various quantities.